

lecture 19  $\frac{u}{D}$

$\frac{\nu}{D}$

Nov 14, 2018

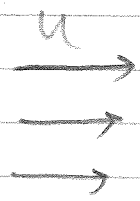
$$\frac{\partial \vec{v}}{\partial t} + (\vec{v} \cdot \nabla) \vec{v} = -\frac{\nabla p}{\rho} + \nu \nabla^2 \vec{v}$$

advection of momentum

viscous diffusion of momentum

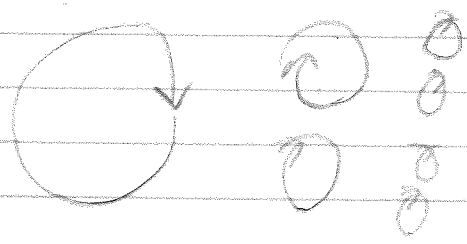
$$Re = \frac{\text{inertial forces}}{\text{viscous forces}} = \frac{UD}{\nu} = \frac{\rho UD}{\mu}$$

$$\frac{u/D}{\nu/D} = \frac{UD}{\nu}$$



$\rho$

Turbulent cascade



$$Re = \frac{UD}{\nu}$$

$$Re = 1$$

viscous effects dominate  
dissipate energy to heat

Kolmogorov (1941)

small scale  $\eta$   
eddy

2 variables:  $\nu, \epsilon$   
 $\left[ \frac{m^2}{s} \right], \left[ \frac{m^3}{s^3} \right]$

$$\eta = \left( \frac{\nu^3}{\epsilon} \right)^{1/4}$$

$$\hat{u}_\eta = \left( \frac{\nu}{\epsilon} \right)^{1/2}$$

$$Re = \left( \frac{\eta}{\hat{u}_\eta} \right) \hat{u}_\eta = 1$$

eg. paper

$$R = 10 \text{ cm}$$

$$\varepsilon = 5 \frac{\text{m}^2}{\text{s}^3}$$

$$f = 4 \text{ Hz}$$

$$\nu = 10^{-6} \frac{\text{m}^2}{\text{s}} \Rightarrow \eta = 20 \mu\text{m}$$

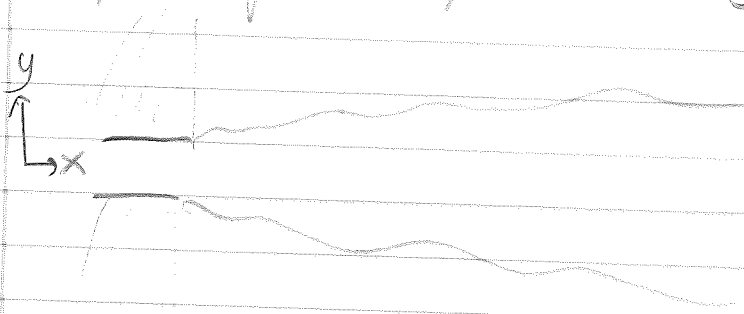
$2R = 10^4$  cells across to resolve smallest eddies

↑

in 3D:  $(10^4)^3 = 10^{12}$  cells that's a lot!

Boundary layer equations

2D, incompressible, turbulent jet from slot



Define length scales

$l_x$ : length over which  $\bar{u}$  changes along  $x$  significantly

$$\bar{u} \quad l_x \quad \frac{\bar{u}}{2}$$

$l_y$ : change of  $\bar{u}$  along  $y$  by same amount

$$\frac{l_y}{l_x} \ll 1 \quad \text{thin jet}$$

①

$$\frac{l_y(x)}{l_x(x)} \ll 1 \quad \text{locally thin}$$

$$Re(x) = \frac{u(x) l_y(x)}{\nu} \gg 1 \quad \text{local high Re}$$

where  $u(x) = \text{peak velocity (centerline)}$

continuity:  $\frac{\partial \bar{u}}{\partial x} + \frac{\partial \bar{v}}{\partial y} = 0$        $\frac{u}{l_x} = \frac{v}{l_y}$        $v = u \frac{l_y}{l_x}$  ( $V \ll u$ )

x-comp:  $\bar{u} \frac{\partial \bar{u}}{\partial x} + \bar{v} \frac{\partial \bar{u}}{\partial y} = -\frac{1}{\rho} \frac{d\bar{p}}{dx} + \nu \left( \frac{\partial^2 \bar{u}}{\partial x^2} + \frac{\partial^2 \bar{u}}{\partial y^2} \right) - \overline{\frac{du^2}{dx}} - \overline{\frac{duv}{dy}}$

$$\frac{u^2}{l_x} \quad \frac{u \Delta \left( \frac{u}{l_x} \right)}{l_x} \quad \frac{1}{\rho} \frac{u^2}{l_x} \quad \frac{\nu u}{l_x^2} \quad \frac{\nu u}{l_y^2} \quad \frac{u^2}{l_x} \quad \frac{u^2}{l_y}$$

②

$$\frac{u^2}{l_x} \quad | \quad | \quad | \quad \frac{\nu}{u l_y} \frac{l_y}{l_x} \quad \frac{\nu}{u l_y} \frac{l_y}{l_y} \quad \frac{u^2}{u^2} \quad \frac{u^2 l_y}{u^2 l_y}$$

$Re \ll 1$       assume  $\nu$  is small      make transition

$\frac{u^2}{u^2} \frac{l_x}{l_y} \sim 1$  for turbulence to be relevant

$$\frac{u}{u} \sim \sqrt{\frac{l_y}{l_x}}$$

③  $\bar{u} \frac{\partial \bar{u}}{\partial x} + \bar{v} \frac{\partial \bar{u}}{\partial y} = -\frac{1}{\rho} \frac{d\bar{p}}{dx} - \overline{\frac{du^2}{dy}}$

→ viscous stress is much less than Reynolds stress  
by a ratio of  $\frac{1}{Re}$

→ normal Reynolds stress  $\ll$  shear Reynolds stress

comp  $u \frac{d\bar{v}}{dx} + v \frac{d\bar{u}}{dy} = -\frac{1}{\rho} \frac{dp}{dy} + \nu \left( \frac{d^2 \bar{v}}{dx^2} + \frac{d^2 \bar{u}}{dy^2} \right) - \frac{d\overline{uv}}{dx} - \frac{d\overline{v^2}}{dy}$

$\frac{uL}{L_y}$   $\frac{u^2}{L_y} \left(\frac{L_y}{L_x}\right)^2$   $\frac{u^2}{L_y} \left(\frac{L_y}{L_x}\right)^2$   $\frac{u^2}{L_y}$   $\frac{\nu u L_y}{L_x^3}$   $\frac{\nu u}{L_x L_y}$   $\frac{u^2}{L_x}$   $\frac{u^2}{L_y}$

$\frac{u^2}{L_y}$   $\left(\frac{L_y}{L_x}\right)^2$   $\left(\frac{L_y}{L_x}\right)^2$   $1$   $\frac{\nu}{u L_y} \left(\frac{L_y}{L_x}\right)^3$   $\frac{\nu}{u L_y} \left(\frac{L_y}{L_x}\right)$   $\left(\frac{L_y}{L_x}\right)^2$   $\left(\frac{L_y}{L_x}\right)$

$$\frac{dp}{dy} = 0$$

$$p = p(x)$$