

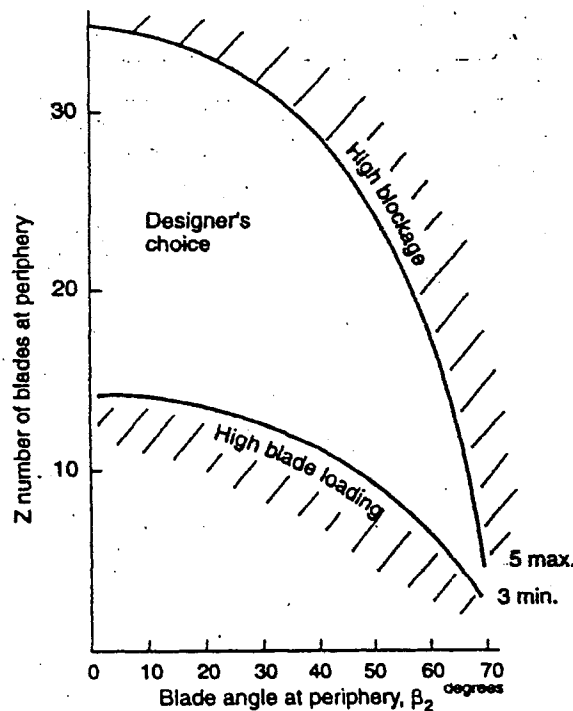
A radial flow compressor impeller is to be designed with no preswirl at the inlet, with $C_{2r} = C_1$ and with the following conditions to be met:

- the flow coefficient at the impeller exit $\Phi_2 = 0.4$
- the impeller tip velocity $U_2 = 300 \text{ m/s}$
- the inlet hub to outlet diameter ratio $d_{h,1}/d_2 = 0.3$
- the relative velocity ratio $W_2/W_{sh,2} = 0.75$
- the slip factor $\sigma = 0.78$
- the impeller outlet blade angle $= 50^\circ$

The flowing medium is air which can be considered as a perfect gas with $C_p = 1005 \text{ J/(kg}\cdot\text{K)}$, $\gamma = 1.4$.

For the above conditions calculate the following:

- the loading coefficient ψ
- the ratio of the inlet shroud-to-hub diameter
- the number of impeller blades corresponding to the prescribed slip factor. In reference to the figure below, is the calculated number of blades a reasonable choice?



We can add further design specification to the problem; namely:

- the impeller outlet speed Mach number $= 0.7$
- the inlet total pressure $P_{01} = 100 \text{ kPa}$
- the impeller total pressure ratio $P_{02}/P_{01} = 1.3$
- the mass flow rate through the impeller $\dot{m} = 20 \text{ kg/s}$

For these additional operating conditions, calculate the following:

- the total-to-total efficiency
- the polytropic efficiency
- the impeller outlet diameter and the inlet hub and shroud diameters.
- the impeller rotational speed in RPM
- the outlet impeller width b_2

Radial compressor impeller

no prewhirl at inlet $c_1 = c_x$

$$c_{2r} = c_1$$

$$\Phi = 0.4 = \frac{c_{2r}}{u_2}$$

$$u_2 = 300 \text{ m/s}$$

$$\frac{d_{h1}}{d_2} = 0.3$$

$$W_2/W_{sh1} = 0.75$$

$$\text{slip factor } \sigma = 0.78$$

$$\text{blade angle } \leftarrow \beta'_2 = 50^\circ \text{ backward}$$

air

$$c_p = 1005 \frac{\text{J}}{\text{kg K}}$$

$$R = 287$$

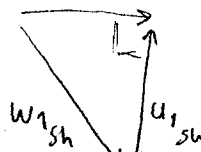
$$\gamma = 1.4$$

Calculate a) ψ , b) $\frac{d_{sh1}}{d_{h1}}$, c) Z

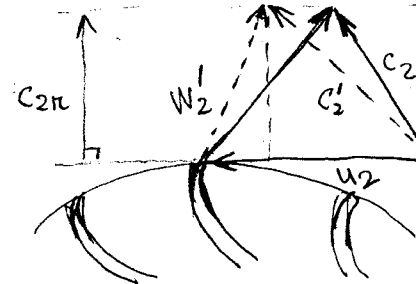
number of blades

impeller inlet (@ shroud)

$$c_1 = c_x$$



impeller outlet



$$a) \psi = \frac{\Delta W_c}{u_2^2}, \Delta W_c = u_2 c_{\theta 2} - u_1 c_{\theta 1}$$

use the impeller outlet blade speed

$$\text{slip factor } \sigma = 0.78 = \frac{c_{\theta 2}}{c_{\theta 2s}} \rightarrow c_{\theta 2} = \sigma c_{\theta 2s}$$

$$\Phi = \frac{c_{2r}}{u_2} = 0.4 \rightarrow c_{2r} = \Phi u_2 = 0.4 \times 300 \text{ m/s} = 120 \frac{\text{m}}{\text{s}}$$

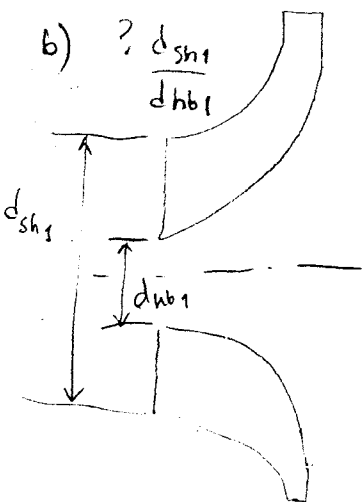
$$\text{Theoretical } W_2' = \frac{c_{2r}}{\cos \beta'_2} = \frac{120}{\cos 50^\circ} = 186.7 \text{ m/s}$$

$$c'_{\theta 2} = u_2 - W_2' \sin \beta'_2 = 300 - 186.7 \sin 50^\circ = 157 \text{ m/s}$$

$$c_{\theta 2} = \sigma c'_{\theta 2} = 0.78 \times 157 = 122.5 \text{ m/s}$$

$$\psi = \frac{c_{\theta 2}}{u_2} = \frac{122.5 \text{ m/s}}{300 \text{ m/s}} = 0.408 \rightarrow \text{moderately loaded}$$

($\psi > 0.5$ heavily loaded)
($\psi < 0.3$ lightly loaded)



$$\frac{d_{h1}}{d_2} = 0.3 \rightarrow \frac{d_{sh1}}{d_{h1}} = \frac{d_{sh1}}{d_2} \frac{d_2}{d_{h1}} = \left(\frac{d_{sh1}}{d_2} \right) \frac{1}{0.3}$$

$$u_2 = \omega r_2 = \omega \frac{d_2}{2}$$

$$u_{sh1} = \omega \frac{d_{sh1}}{2}$$

$$\Rightarrow \frac{d_{sh1}}{d_2} = \frac{u_{sh1}}{u_2}$$

$$u_{sh1} = \sqrt{W_{sh1}^2 - c_1^2}, c_1 = c_{1x} = c_{2r} = 120 \text{ m/s}$$

find w_{sh1} :

$$\frac{w_2}{w_{sh1}} = 0.75 \quad , \quad \text{find } w_2 : \quad w_2 = \sqrt{c_{2n}^2 + w_{2\theta}^2} = \sqrt{c_{2n}^2 + (u_2 - c_{2\theta})^2}$$

$$= \sqrt{120^2 + (300 - 122.5)^2} = 214.3 \text{ m/s}$$

$$w_{sh1} = \frac{w_2}{0.75} = \frac{214.3}{0.75} = 285.7 \text{ m/s}$$

$$u_{sh1} = \sqrt{w_{sh1}^2 - c_1^2} = \sqrt{285.7^2 - 120^2} = 259.3 \text{ m/s}$$

$$\frac{d_{sh1}}{d_2} = \frac{u_{sh1}}{u_2} = \frac{259.3}{300} = 0.864$$

$$\boxed{\frac{d_{sh1}}{d_{h1}}} = \frac{d_{sh1}}{d_2} \cdot \frac{1}{0.3} = \frac{0.864}{0.3} = 2.88$$

c) ? Z = number of blades

$$\sigma = 0.78 = \frac{C_{\theta 2}}{C_{\theta 2}'}$$

use for example Wiesner correl. $\sigma = 1 - \frac{u_2}{C_{\theta 2}'} \frac{\sqrt{\cos \beta_2'}}{Z^{0.7}}$

$$Z^{0.7} = \frac{1}{1 - \sigma_w} \frac{u_2}{C_{\theta 2}'} \sqrt{\cos \beta_2'} = \frac{1}{1 - 0.78} \frac{300}{157} \sqrt{\cos 50^\circ} = 6.96$$

$$Z = 16 \text{ blades}$$

in fig. for $\beta_2 = 50^\circ$: $Z_{min} = 9$ blades (high blade loading)

$Z_{max} = 24$ " (high blockage effect)

$$M_{u2} = \frac{u_2}{\sqrt{\gamma R T_2}} = 0.7$$

$$p_{01} = 100 \text{ kPa}$$

$$\frac{p_{02}}{p_{01}} = 1.3$$

$$\dot{m} = 20 \text{ kg/s}$$

calculate: d) η_{tt}

e) $\eta_{p,tt}$

f) d_z, d_{sh1}, d_{ab1}

g) $N [\text{RPM}]$

h) b_z

usually it's for the whole stage or the whole compressor but in this case we know only about the impeller!

$$d) \eta_{tt} = \frac{h_{02s} - h_{01}}{h_{02} - h_{01}} =$$

$$= \frac{T_{02s} - T_{01}}{T_{02} - T_{01}} = \frac{\left(\frac{T_{02s}}{T_{01}}\right) - 1}{\left(\frac{T_{02}}{T_{01}}\right) - 1}$$

$$\text{where } \frac{T_{02s}}{T_{01}} = \left(\frac{p_{02}}{p_{01}}\right)^{\frac{\gamma-1}{\gamma}} = (1.3)^{1/3.5} = 1.0778$$

$$T_{02} = T_2 + \frac{c_2^2}{2c_p}$$

$$\text{where } c_2^2 = \sqrt{c_{2r}^2 + c_{2o}^2} = \sqrt{120^2 + 122.5^2} = 171 \text{ m/s}$$

$$\text{2 get } T_2 \text{ from } M_{u2} = 0.7 \Rightarrow \sqrt{\gamma R T_2} = \left(\frac{u_2}{M_{u2}}\right)^2$$

$$T_2 = \frac{1}{\gamma R} \left(\frac{u_2}{M_{u2}}\right)^2 = \frac{1}{1.4 \times 287 \frac{\text{J}}{\text{kg K}}} \left(\frac{300}{0.7}\right)^2 = 457.1 \text{ K}$$

$$T_{02} = T_2 + \frac{c_2^2}{2c_p} = 457.1 + \frac{171^2}{2 \times 1005} = 471.7 \text{ m/s}$$

$$\Delta W_c = h_{02} - h_{01} = c_p (T_{02} - T_{01}) = u_2 c_{\theta 2} - u_1 c_{\theta 1}^0 = 300 \times 122.5 = 36750 \frac{\text{J}}{\text{kg}}$$

$$\eta_{tt} = \frac{\frac{T_{02s}}{T_{01}} - 1}{\frac{T_{02}}{T_{01}} - 1} = \frac{1.0778 - 1}{\frac{471.7}{435.1} - 1} = 92.5 \% \quad \text{isentropic total-to-total efficiency}$$

e) ? $\eta_{p,tt}$: $\frac{T_{02}}{T_{01}} = \left(\frac{p_{02}}{p_{01}}\right)^{\frac{R}{C_p} \eta_{p,tt}}$

$\ln \frac{T_{02}}{T_{01}} = \frac{R}{C_p} \eta_{p,tt} \ln \frac{p_{02}}{p_{01}} \Rightarrow \boxed{\eta_{p,tt}} = \frac{\frac{R}{C_p} \ln \frac{p_{02}}{p_{01}}}{\ln \frac{T_{02}}{T_{01}}} = \frac{\frac{1}{3.5} \ln 1.3}{\ln \left(\frac{471.7}{435.1}\right)} = \boxed{92.8\%}$

polytropic total-to-total efficiency:

Note $\eta_{s,tt} < \eta_{p,tt}$ for a compressor

f) ? d_2, d_{sh1}, d_{hb1} :

$\dot{m} = 20 \frac{\text{kg}}{\text{s}} = \rho_1 A_1 c_{1x} = \rho_2 A_2 c_{2x}$

where $A_1 = \frac{\pi}{4} (d_{sh1}^2 - d_{hb1}^2)$

and $A_2 = \pi d_2 b_2$

find p_1 : $p_1 = \frac{P_1}{RT_1}$

$c_1 = 120 \frac{\text{m}}{\text{s}}$

$T_1 = T_{01} - \frac{c_1^2}{2C_p} = 435.1 - \frac{120^2}{2 \cdot 1005} = 427.9 \text{ K}$

$M_1 = \frac{c_1}{\sqrt{\gamma R T_1}} = \frac{120}{\sqrt{1.4 \cdot 287 \cdot 427.9}} = 0.29$

$P_1 = P_{01} \left[1 + \frac{\gamma-1}{2} M_1^2\right]^{-\frac{\gamma}{\gamma-1}} = 100 \left[1 + \frac{1.4-1}{2} 0.29^2\right]^{-\frac{1.4}{0.4}} = 94.33 \text{ kPa}$

$\rho_1 = \frac{P_1}{RT_1} = \frac{94.33 \cdot 10^3}{287 \cdot 427.9} = 0.768 \frac{\text{kg}}{\text{m}^3}$

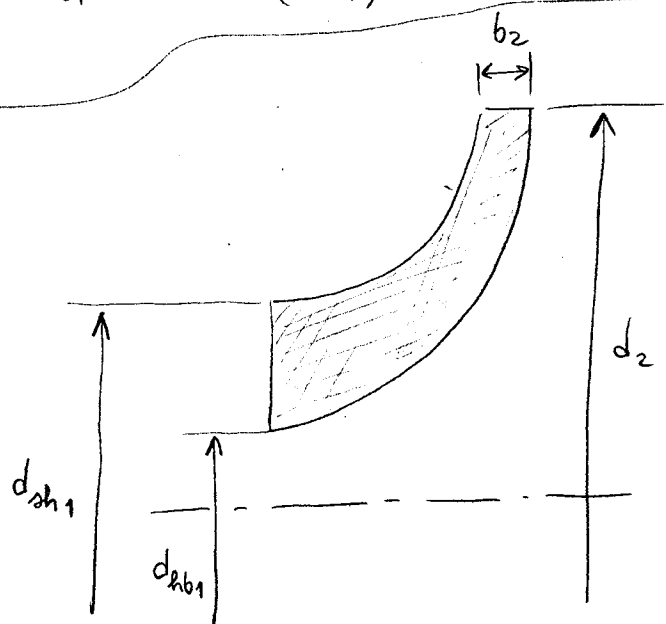
$\rightarrow A_1 = \frac{\dot{m}}{\rho_1 c_{1x}} = \frac{20 \frac{\text{kg}}{\text{s}}}{0.768 \frac{\text{kg}}{\text{m}^3} 120 \frac{\text{m}}{\text{s}}} = 0.217 \text{ m}^2 = \frac{\pi}{4} (d_{sh1}^2 - d_{hb1}^2)$

$\begin{cases} d_{sh1}^2 - d_{hb1}^2 = \frac{4 A_1}{\pi} = 0.27631 \text{ m}^2 \\ \frac{d_{sh1}}{d_{hb1}} = 2.88 \quad (\text{from part b}) \end{cases}$

$d_{sh1} = 2.88 d_{hb1} \Rightarrow (2.88^2 - 1) d_{hb1}^2 = 0.27631 \Rightarrow \boxed{d_{hb1} = 0.1946 \text{ m}}$

$\boxed{d_{sh1}} = 2.88 \times 0.1946 = \boxed{0.5605 \text{ m}}$

$\frac{d_{hb1}}{d_2} = 0.3 \text{ (given)} \Rightarrow \boxed{d_2} = \frac{d_{hb1}}{0.3} = \frac{0.1946}{0.3} = \boxed{0.6488 \text{ m}}$



g) ? N [RPM]

$$u_2 = \omega r_2 = \frac{2\pi N}{60} \cdot \frac{d_2}{2}$$

$$\Rightarrow \boxed{N} = \frac{60 u_2}{\pi d_2} = \frac{60 \cdot 300}{\pi \cdot 0.6488} = \boxed{8831 \text{ RPM}}$$

h) ? b_2 (outer impeller width):

$$\dot{m} = \rho_2 A_2 c_{2r} \quad \text{where } A_2 = \pi d_2 b_2$$

find ρ_2 :

$$M_2 = \frac{c_2}{\sqrt{\gamma R T_2}} = \frac{171.5}{\sqrt{1.4 \times 287 \times 457.1}} = 0.4$$

$$p_{02} = 1.3 p_{01} = 130 \text{ kPa}$$

$$p_2 = p_{02} \left[1 + \frac{\gamma-1}{2} M_2^2 \right]^{-\frac{\gamma}{\gamma-1}} = 130 \left[1 + \frac{1.4-1}{2} M_2^2 \right]^{-\frac{1.4}{0.4}} = 116.4 \text{ kPa}$$

$$\rho_2 = \frac{p_2}{R T_2} = \frac{116.4 \times 10^3}{287 \times 457.1} = 0.887 \frac{\text{kg}}{\text{m}^3}$$

$$\text{hence } A_2 = \frac{\dot{m}}{\rho_2 c_{2r}} = \frac{20}{0.887 \cdot 120} = 0.1878 \text{ m}^2 = \pi d_2 b_2$$

$$\Rightarrow \boxed{b_2} = \frac{A_2}{\pi d_2} = \frac{0.1878}{\pi \cdot 0.6488} = \boxed{0.0921 \text{ m}}$$

i) $N_{s1} = \frac{2\pi N \sqrt{\dot{V}_1}}{60 (h_{02} - h_{01})^{3/4}} \quad \text{where } h_{02} - h_{01} = c_p (T_{02} - T_{01})$

$$\dot{V}_1 = A_1 c_{1x} = \frac{\dot{m}}{\rho_1} = \frac{20}{0.768} = 26.04$$

$$\boxed{N_{s1}} = \frac{2\pi \cdot 8831 \sqrt{26.04}}{60 [1005 (471.7 - 435.1)]^{3/4}} = \boxed{1.78}$$

~~Not if we use $\dot{V}_2$~~

Fig. 5.20: for $\beta_2 = 50^\circ$, $M_{u2} = 0.7$, $\phi = \frac{c_{x1}}{u_2} = 0.4$

$$\eta_{P,H} \approx 93\% \text{ corresponds to } N_{s1} \approx 0.8$$

while in the present case $\eta_{P,H} = 93\%$ corresponds to $N_{s1} = 1.78$,
Thus, the performance characteristics in fig. 5.20 apply for a different impeller.