

Sept. 26
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Recap

Constitutive Equation relates:

Flux - Transport - Force Gradient
Property

Heat:	$q = -k \cdot \vec{\nabla} T$	(Fourier)
Momentum:	$\tau_{yx} = \mu \frac{dv_x}{dy}$	(Newton's Law of Viscosity)
Mass:	$J_A = -D_{AB} \vec{\nabla} S_A$	(Fick)

Unified 1D Constitutive Eq.

$f_y = -D \frac{db}{dy}$	$f_y \dots$ flux of property in y direction
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$\alpha = \nu = D_{AB} \equiv D$ $D [] \frac{m^2}{s} \dots$ diffusivity
 $b \dots$ property concentration

Species Diffusion

molar flux observed by stationary observer

has a convective and diffusive flux component

flux relation	$N_i = \begin{cases} C_i \vec{v} + \vec{J}_i \\ C_i \vec{v}^{(M)} + \vec{J}_i^{(M)} \end{cases}$	based on mass average velocity \vec{v}
		based on molar average velocity $\vec{v}^{(M)}$

Binary System ; A, B

$$N = N_A + N_B$$

total convective flux
relative to stationary observer

$$= C v^{(M)}$$

$$C = C_A + C_B$$

total concentration

(drop vector for simplicity)
i.e. consider 1D transport

\Rightarrow molar average velocity:

$$v^{(M)} = \frac{N_A + N_B}{C}$$

We substitute $v^{(M)}$ into the
flux relation: $N_A = C_A v^{(M)} + J_A$

$$\Rightarrow N_A = J_A + \frac{C_A}{C} (N_A + N_B)$$

Next subst. for J_A from Deen Table (1-3) eq. D

mole fraction
(Fick's Law)

$$\Rightarrow (1) \quad N_A = \underbrace{-C D_{AB} \frac{dx_A}{dz}}_{\text{diffusive flux component of A}} + \underbrace{\frac{C_A}{C} (N_A + N_B)}_{\text{convective flux component}}$$

analogous for B:

$$(2) \quad N_B = -C D_{BA} \frac{dx_B}{dz} + \frac{C_B}{C} (N_A + N_B)$$

To solve (1) or (2) we need $N_A = f(N_B)$ $i = A, B$

Ex: $N_A = -N_B$ (equimolar counterdiff.) $\Rightarrow N_i = J_i^{(M)}$
 $\rightarrow N_A + N_B = 0$

Two useful reference frames in mixtures are the *mass-average velocity* \mathbf{v} and the *molar-average velocity* $\mathbf{v}^{(M)}$. They are defined as

$$\mathbf{v} = \sum_{i=1}^n \omega_i \mathbf{v}_i, \quad \mathbf{v}^{(M)} = \sum_{i=1}^n x_i \mathbf{v}_i \quad (1.2-6)$$

where ω_i and x_i are the mass fraction and mole fraction of species i , respectively, and n is the number of chemical species in the mixture. The mass and mole fractions are related to the total mass density (ρ) and total molar concentration (C) by

$$\omega_i = \frac{\rho_i}{\rho} = \frac{\rho_i}{\sum_{i=1}^n \rho_i}, \quad x_i = \frac{C_i}{C} = \frac{C_i}{\sum_{i=1}^n C_i} \quad (1.2-7)$$

The various diffusional fluxes defined using \mathbf{v} or $\mathbf{v}^{(M)}$ are listed in Table 1-2.

Table 1-2
Flux of Species i in Various Reference Frames and Units

Reference velocity	Molar units	Mass units
0	N_i	n_i
\mathbf{v}	\mathbf{J}_i	\mathbf{j}_i
$\mathbf{v}^{(M)}$	$\mathbf{J}_i^{(M)}$	$\mathbf{j}_i^{(M)}$

Table 1-3
Fick's Law for Binary Mixtures of A and B

Reference velocity	Mass units	Molar units
\mathbf{v}	$\mathbf{j}_A = -\rho D_{AB} \nabla \omega_A$ (A)	$\mathbf{J}_A = \frac{\rho D_{AB}}{M_A} \nabla \omega_A$ (B)
$\mathbf{v}^{(M)}$	$\mathbf{j}_A^{(M)} = -C M_A D_{AB} \nabla x_A$ (C)	$\mathbf{J}_A^{(M)} = -C D_{AB} \nabla x_A$ (D)

Heat Flux

Constitutive Eq.

Fourier's Law: $\vec{q} = -k \vec{\nabla} T$; Thermal conductivity
 k is isotropic

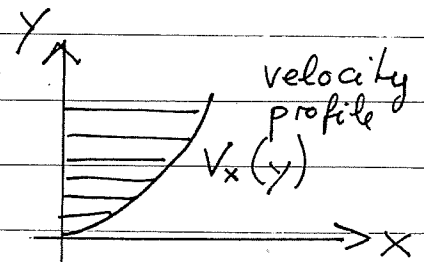
$\vec{q} = -\underline{\underline{\kappa}} \vec{\nabla} T$; anisotropic materials
 \rightarrow conductivity tensor $\underline{\underline{\kappa}}$

Heat flux normal (\vec{n}) to a surface :

scalar: $q_n = \vec{n} \cdot \vec{q} = -k (\vec{n} \cdot \vec{\nabla} T)$

Momentum Flux

unidirectional flow: $\vec{v} = v_x(y) \vec{e}_x$



\Rightarrow Viscous stress of Newtonian fluid

$$\tau_{yx} = \mu \frac{dv_x}{dy} \quad \text{Newton's Law of Viscosity}$$

Newtonian fluids in 3D :

$$\underline{\underline{\tau}} = \mu \left(\underline{\underline{\nabla v}} + (\underline{\underline{\nabla v}})^t \right) ; \quad t \dots \text{transpose of matrix}$$

"velocity gradient": $\underline{\underline{\nabla v}}$ (velocity dyad) =
$$\begin{pmatrix} \frac{\partial v_x}{\partial x} & \frac{\partial v_x}{\partial y} & \frac{\partial v_x}{\partial z} \\ \frac{\partial v_y}{\partial x} & \frac{\partial v_y}{\partial y} & \frac{\partial v_y}{\partial z} \\ \frac{\partial v_z}{\partial x} & \frac{\partial v_z}{\partial y} & \frac{\partial v_z}{\partial z} \end{pmatrix} ; \quad v_i = v_i(x, y, z) \\ i = x, y, z$$