

EXAMPLE 3.2-2 Reversible Homogeneous Reaction in a Liquid This problem is similar to Example 3.2-1, except that the reaction now is reversible. Also, as shown in Fig. 3-3, the open boundary (where the concentrations are fixed at C_{A0} and C_{B0}) is now at $y = 0$ and the impermeable one is at $y = L$. The reversibility of the reaction requires that both species concentrations be considered simultaneously. Nonetheless, as will be shown, the two conservation equations can be uncoupled.

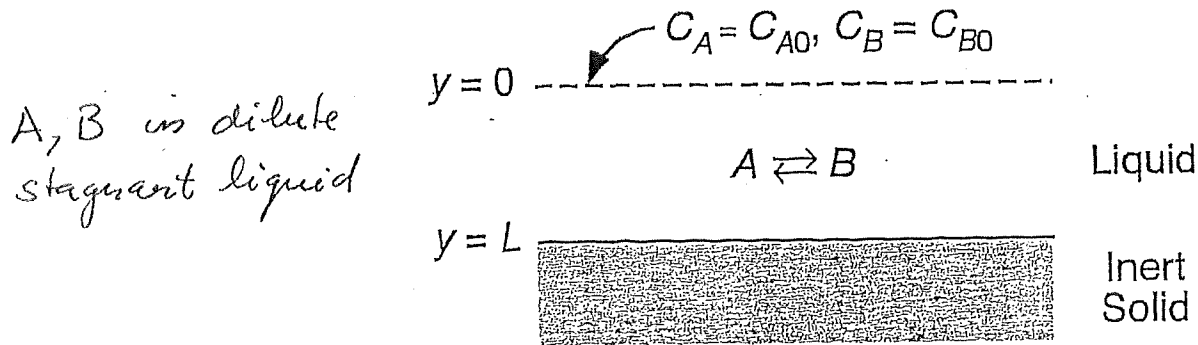


Figure 3-3. Steady diffusion in a liquid film with a reversible homogeneous reaction.

Start with same Conservation Eq. as for 3.2-1, but for both components

coupled
conserv.
eq.

$$\begin{aligned} 0 &= D_A \frac{d^2 C_A}{dy^2} + R_{VA} \\ 0 &= D_B \frac{d^2 C_B}{dy^2} + R_{VB} \end{aligned}$$

$\nearrow -R_{VA}$

1st order kinetics:

$$\begin{aligned} R_{VA} &= k_{-1} C_B - k_1 C_A \\ &= k_1 (K C_B - C_A) \\ &= -R_{VB} \end{aligned}$$

equil. const: $K = \frac{k_{-1}}{k_1}$

Boundary Conditions

BC1: $C_A(y=0) = C_{A0}$, $C_B(y=0) = C_{B0}$

BC2: $\frac{dC_A}{dy}(y=L) = 0$, $\frac{dC_B}{dy}(y=L) = 0$ impermeable inert solid

Sum of the two conservation eqs yields:

$$0 = D_A \frac{d^2 C_A}{dy^2} + D_B \frac{d^2 C_B}{dy^2}$$

which after integrations (twice with BCs) provides a relationship between C_A and C_B , namely:

$$C_B(y) = \frac{D_A}{D_B} (C_{A0} - C_A(y)) + C_{B0} \quad (*)$$

continue Ex 3.2-2

We return to our (coupled) conservation eq.

$$0 = D_A \frac{d^2 C_A(y)}{dy^2} + R_{VA} \quad ; \quad R_{VA} = k_1 (K C_B - C_A)$$

subst (*) $\xrightarrow{\uparrow}$

$$\Rightarrow 0 = D_A \frac{d^2 C_A}{dy^2} + k_1 \left(K \left(\frac{D_A}{D_B} [C_{A0} - C_A] + C_{B0} \right) - C_A \right)$$

\rightarrow diff. eq. in $C_A(y)$ only

Conservation Eq.

$$0 = D_A \frac{d^2 C_A(y)}{dy^2} - k_1 \left(\frac{K D_A}{D_B} + 1 \right) C_A(y) + k_1 K \left(\frac{D_A}{D_B} C_{A0} + C_{B0} \right)$$

This equation can be rewritten with the following dimensionless parameters:

Damköhler numbers for forward and backward reactions =

$$\begin{cases} \alpha \equiv \frac{k_1 L^2}{D_A} \\ \beta \equiv \frac{k_{-1} L^2}{D_B} \end{cases}$$

$$\eta = \frac{y}{L}, \quad \Theta_A = \frac{C_A}{C_{A0}}, \quad \Theta_B = \frac{K C_B}{C_{A0}}$$

Dimensionless Conservation Eq.

$$\frac{d^2 \Theta_A}{d\eta^2} = (\alpha + \beta) \Theta_A - (\alpha \eta + \beta)$$

with $\eta_1 \equiv \frac{K C_{B0}}{C_{A0}}$ (determines direction of reaction)

continue Ex 3.2-2

(3)

The dimensionless conservation eq. above with

$$BC(1) : \Theta_A(0) = 1$$

$$BC(2) : \frac{d\Theta_A}{d\eta}(1) = 0 \quad (\text{impermeable solid})$$

yields the following solutions

$$\Theta_A(\eta) = \left[\frac{\alpha\eta + \beta}{\alpha + \beta} \right] + \left[\frac{\alpha(1-\eta)}{\alpha + \beta} \right] \times$$

$$\times \left[\cosh(\eta\sqrt{\alpha+\beta}) - \tanh(\sqrt{\alpha+\beta}) \sinh(\eta\sqrt{\alpha+\beta}) \right]$$

and analogous for $\Theta_B(\eta)$ (see text eq. 3.2-25)

Examine the solution for very fast reactions, i.e.,

$$\boxed{\alpha \rightarrow \infty}$$

with $\frac{\beta}{\alpha} = \text{constant}$

(which leaves K to be constant)

$$\Rightarrow \tanh x \rightarrow 1$$

$$\cosh x - \sinh x \rightarrow e^{-x}$$

$$\Rightarrow \boxed{\Theta_A(\eta) = \left[\frac{\eta + (\beta/\alpha)}{1 + (\beta/\alpha)} + \left[\frac{1-\eta}{1 + (\beta/\alpha)} \right] e^{-\eta\sqrt{\alpha+\beta}} \right]}$$

and equivalent eq. for $\Theta_B(\eta)$

Example 3.2-2: Reversible Homogeneous Reaction in a Liquid

$$\eta = \frac{y}{L}, \quad \theta_A = \frac{C_A}{C_{A0}}, \quad \theta_B = \frac{K C_B}{C_{A0}} \quad (3.2-20)$$

The dimensionless concentrations have been chosen so that $\theta_A = \theta_B$ at equilibrium. After changing variables and eliminating C_B as described above, Eq. (3.2-12) and its boundary conditions become

Conservation Governing Eq.

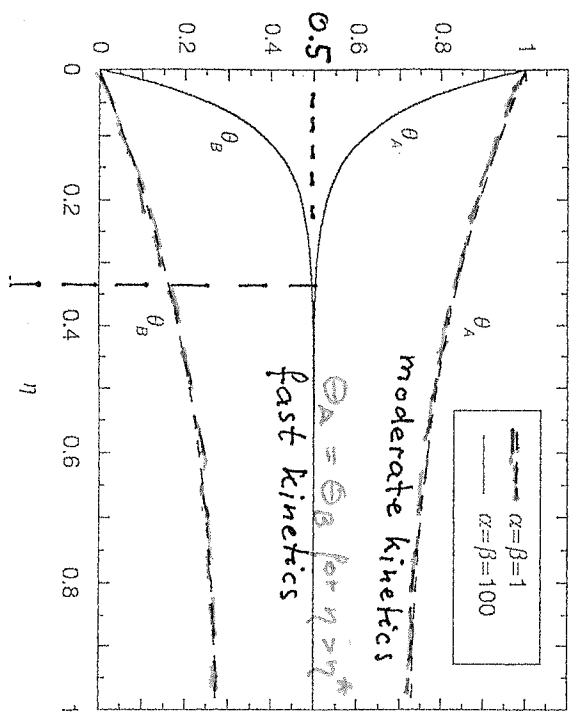
$$\frac{d^2 \theta_A}{d\eta^2} = (\alpha + \beta) \theta_A - (\alpha \gamma + \beta) \quad (3.2-21)$$

(Dimensionless) BCs $\theta_A(0) = 1, \quad \frac{d\theta_A}{d\eta}(1) = 0.$ (3.2-22)

The dimensionless parameters that appear are

Damköhler $\alpha = \frac{k_1 L^2}{D_A}, \quad \beta = \frac{k_{-1} L^2}{D_B}, \quad \gamma = \frac{K C_{B0}}{C_{A0}}.$ (3.2-23)

Plots of Eqs. (3.2-24) and (3.2-25) for moderate and fast reactions (with $\gamma=0$) are shown in Fig. 3-4. For $\alpha = \beta = 1$ the reaction $A \rightarrow B$ proceeds at significant rates throughout the film, whereas for $\alpha = \beta = 100$ there are distinct reaction and equilibrium zones, as discussed above.



for $\beta \neq 100$:
 non equilib. zone η^* equil. zone

Fig. 3-4. Plots of θ_A and θ_B for moderate and fast reactions (with $\gamma=0$) are shown in Fig. 3-4. For $\alpha = \beta = 1$ the reaction $A \rightarrow B$ proceeds at significant rates throughout the film, whereas for $\alpha = \beta = 100$ there are distinct reaction and equilibrium zones, as discussed above.

The solution to Eq. (3.2-21) is

$$\theta_A(\eta) = \left[\frac{\alpha \gamma + \beta}{\alpha + \beta} \right] + \left[\frac{\alpha(1 - \gamma)}{\alpha + \beta} \right] \left[\cosh(\eta \sqrt{\alpha + \beta}) - \tanh(\sqrt{\alpha + \beta}) \sinh(\eta \sqrt{\alpha + \beta}) \right]. \quad (3.2-24)$$

As in Example 3.2-1, the finite film thickness motivates the use of hyperbolic functions rather than exponentials. The corresponding result for species B is

$$\theta_B(\eta) = \left[\frac{\alpha \gamma + \beta}{\alpha + \beta} \right] - \left[\frac{\beta(1 - \gamma)}{\alpha + \beta} \right] \left[\cosh(\eta \sqrt{\alpha + \beta}) - \tanh(\sqrt{\alpha + \beta}) \sinh(\eta \sqrt{\alpha + \beta}) \right]. \quad (3.2-25)$$

These results are exact for all values of the three parameters.

Approx: Very fast reaction $\alpha \rightarrow \infty$

$$\theta_A(\eta) = \left[\frac{\gamma + (\beta/\alpha)}{1 + (\beta/\alpha)} \right] + \left[\frac{1 - \gamma}{1 + (\beta/\alpha)} \right] \frac{e^{-\eta \sqrt{\alpha + \beta}}}{e^{-\eta \sqrt{\alpha + \beta}}} \quad (3.2-26)$$

$$\theta_B(\eta) = \left[\frac{\gamma + (\beta/\alpha)}{1 + (\beta/\alpha)} \right] - \left[\frac{(\beta/\alpha)(1 - \gamma)}{1 + (\beta/\alpha)} \right] \frac{e^{-\eta \sqrt{\alpha + \beta}}}{e^{-\eta \sqrt{\alpha + \beta}}}. \quad (3.2-27)$$

Over most of the film (except near $\eta = 0$) the exponential terms will be negligible, so that

$$\theta_A \approx \left[\frac{\gamma + (\beta/\alpha)}{1 + (\beta/\alpha)} \right] \approx \theta_B. \quad \text{for } \eta \gg \eta^* \quad (3.2-28)$$

fast kinetics

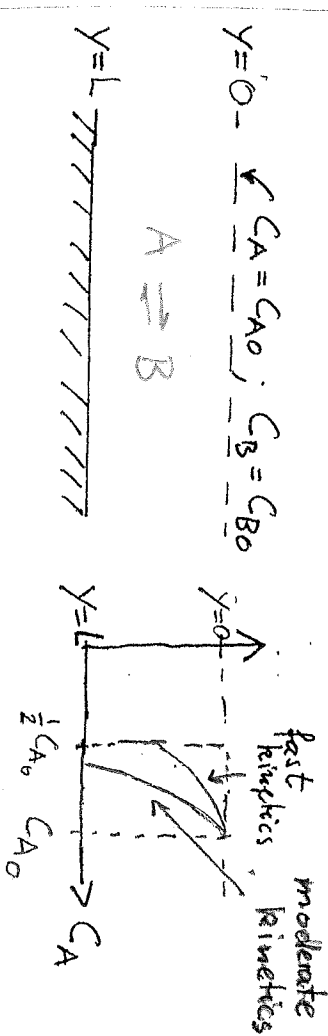


Fig. 3-4. Plots of θ_A and θ_B for moderate and fast reactions (with $\gamma=0$) are shown in Fig. 3-4. For $\alpha = \beta = 1$ the reaction $A \rightarrow B$ proceeds at significant rates throughout the film, whereas for $\alpha = \beta = 100$ there are distinct reaction and equilibrium zones, as discussed above.